# A Decade of Successful Collaborations in Nutritional Compound Process Research and Development

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Abstract: Collaborations between academia and industry are vital for modern industrial research and development projects, combining the best of both worlds to develop sustainable chemical processes. Herein we summarize a number of successful cooperations between DSM Nutritional Products and Swiss academic institutions that have been carried out over approximately the past decade. A wide variety of reactions and processes have been investigated with experts located in Switzerland. New synthetic routes, chemical transformations and reactor concepts have been developed to produce industrially relevant compounds. Additionally the scope of known catalytic systems has been probed and new catalysts showing improved selectivity have been designed, synthesized and tested. We describe how the research was supported by DSM, the parallel in-house investigations and also how the projects were continued and further developed.

Keywords: Catalysis · Fine chemicals · Nutritional ingredients · Sustainable chemical processes · Vitamins



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#### 1. Introduction

The driving force for chemical process research, especially in the fine chemicals' industry, is the development of sustainable, efficient and low-cost production processes for a wide variety of compounds and products. An advantage and challenge of working in the area of vitamins, nutritional ingredients, personal care and aroma chemicals is that many of the active molecules have an eternal lifetime. That is, they have been known and produced for many years (and even decades) and will continue to be needed in the future. Therefore improved processes are always required, but the target is already set very high by the vast amount of existing knowledge of the current systems. In addition, there are always further, as yet uncommercialized compounds, that show a nutritional benefit to both humans and animals, where the development of novel, efficient syntheses is also required. Due to tight project timelines, or perhaps limited existing experience and know-how, it is not always possible or even sensible to investigate all potential ideas in-house. Therefore there is the need to work with experts outside DSM in certain fields. Given the strength and breadth of scientific knowledge in Switzerland, the vast majority of DSM's collaborations in process chemistry can be fulfilled by scientists "just around the corner".

Rather than focus on one particular cooperation, what we have aimed to do in this article is to highlight some of the collaborations undertaken in approximately the past ten years in the field of process research. These projects were initiated for a variety of reasons such as: investigating a specific transformation that was relevant to a running R&D project at DSM, obtaining more indepth understanding of a particular class of reactions or catalysts where there was limited existing in-house knowledge or testing new technologies and emerging fields for relevance to DSM, and fundamental investigations that would hopefully lead to a stepchange in chemical production. In all cases we have sought out local experts in their field for collaborations. In addition, DSM is also approached by academics working in a particular area who are interested in applying their research to DSM's products. Sometimes a mutual project with DSM-funded investigations is initiated immediately; in other cases the collaboration starts slowly by providing materials or analytic recommendations and then grows to a cooperation with masters and PhD students, and postdocs.

#### 2. Heterogeneous Hydrogenation

Catalytic hydrogenation reactions are widely used in all areas of industrial chemical synthesis and are of particular importance in the manufacture of fine chemicals such as vitamins, carotenoids and aroma compounds.<sup>[1]</sup> During the past decades a number of different hydrogenation processes have been developed and implemented, generally using commercial catalysts. One area of particular importance to DSM is the use of selective hydrogenation, such as the reduction of only one functional group in the presence of several others, and especially important, the semi-hydrogenation of alkynes to alkenes (Scheme 1). The search for the next generation of catalysts and hydrogenation processes has been a particularly active area for collaborations, both within Switzerland and elsewhere in Europe.



Scheme 1. An example of industrially relevant semi-hydrogenations of alkynes to alkenes.

The traditional catalyst of choice for alkyne semi-hydrogenation is the Lindlar catalyst, which is palladium deposited on a calcium carbonate support, doped with lead.<sup>[2]</sup> Obtaining high selectivity at high conversions is a particular challenge as competing over-hydrogenation (conversion of the alkene to the corresponding alkane) can occur before the starting alkyne is completely consumed. Whilst the Lindlar catalyst can be incredibly effective, the need for sustainable manufacturing methods requires the replacement of compounds and catalysts, such as those containing lead, with more environmentally friendly alternatives. In addition, the replacement of a batch process with a continuous one would result in significant benefits such as energy recovery and throughput. Therefore DSM has been collaborating with a number of academic institutions throughout Europe in recent years to develop new types of catalysts and catalytic reactors, for example catalysts on porous glass supports,<sup>[3]</sup> and use of alternative enabling technologies such as ultrasound and microwaves for both the catalyst preparation<sup>[4]</sup> and in a hydrogenation reactor.<sup>[5]</sup>

Focusing on joint research projects carried out within Switzerland, the reaction kinetics of the methylbutynol hydrogenation to methylbutenol (Scheme 1.  $1 \rightarrow 2$ , R = Me), an important starting point for the manufacture of vitamins A and E and many other products of relevance to DSM, was studied in detail with the group of Prof. L. Kiwi-Minsker at EPFL.<sup>[6]</sup> The key findings of this study were that the experimental data obtained under the kinetic regime were consistent with the Langmuir-Hinshelwood mechanism. The high alkene selectivity was explained by the two orders of magnitude higher adsorption constant of the alkyne to the catalyst surface, compared with the corresponding alkene. Furthermore, new catalysts for the selective hydrogenation of alkynols (such as methylbutynol) were developed. These catalysts are based on structured sintered metal fibres (SMF), which were coated with an oxide layer of ZnO and/or Al<sub>2</sub>O<sub>2</sub>. Pd-nanoparticles, which act as the active hydrogenation catalyst, were then deposited on the oxide layer.<sup>[7]</sup> The main advantages of these catalysts are that they show high activity and selectivity and additionally are Pb-free and have low Pd-loadings (around 0.5% compared with 5% for a typical Lindlar catalyst). A modified version of these catalysts allowed the selective and sequential hydrogenation of polyenones (hydrogenation of C=C bonds) (Scheme 2).<sup>[8]</sup> The double bond in the  $\gamma$ , $\delta$ -position is hydrogenated initially, followed by the one in the  $\alpha$ , $\beta$ -position; the isolated double bond at the end of the chain is left predominantly untouched. Hydrogenation reactions with these types of catalyst are carried out at 40–230 °C, up to 20 bar pressure and under solvent-free conditions.

A further collaboration in the area of selective semi-hydrogenation of alkynes focused on the development of not only an improved catalyst, but also an improved reactor concept to ensure excellent two-phase mixing between the alkyne and hydrogen gas. A 3D printed porous structured reactor was developed by the group of Prof. P. Rudolf von Rohr at ETH Zurich<sup>[9]</sup> and a suitable catalytic coating was developed at DSM and successfully transferred to the 1<sup>st</sup> and 2<sup>nd</sup> generation tubular reactors.

Initially, metal alloy-based powdered catalysts were used as a prototype for the catalyst development at DSM. The improved



Scheme 2. Sequential reductions of carbon–carbon double bonds using a SMF-catalyst.

preparation procedure was extended to two different designs of structured reactors, called the porous and triangular structures (Fig. 1), which were developed within the project, and tested in the continuous semi-hydrogenation of methylbutynol (1, R = Me).<sup>[10]</sup>

ed conditions was observed for the triangular structured reactor. After 270 h on stream, the TOF decreased by 13% compared to the original value; the original catalyst activity was re-established after a thermal treatment, showing the high stability of the catalytic coating of the structured reactors.<sup>[10b]</sup> The mini-plant setup was continuously improved and has now been transferred to the DSM laboratories (Fig. 2) and additional studies are on-going with further alkyne substrates.



Fig. 1. View of the porous (left) and triangular (right) structured reactors.

Building on the knowledge obtained in the collaboration with EPFL (see above), the metal powders were coated with a primer layer, upon which the palladium could easily be deposited.<sup>[9a,11]</sup> The primer precursor ( $Al_2O_3/ZnO$  and  $CeO_2/ZnO$ ) was then converted to the desired coating material by a subsequent thermal post-treatment. Optimization of primer and Pd-nanoparticle-procedures was carried out by testing parameters such as Pd-loadings, the primer layer thickness and the thermal activation of the final catalyst. Prepared catalysts were tested in batch hydrogenation reactions and the catalysts were fully characterized by a number of different techniques.

The structured reactors were designed at ETH and manufactured by the laser sintering technique which allows for the production of 3D metal supports of nearly any shape. The novel designed structures consist of unit cells, which repeat periodically and allow easily for scaling in length and diameter of reactors. The 2<sup>nd</sup> generation triangular structure (Fig. 1, right) was developed with the desire for an increased surface area, an improved dispersion quality and a reduced pressure drop compared to the porous structure (Fig. 1, left), whilst maintaining a similar porosity. The specific surface area of the triangular structure is more than doubled compared to the porous structure. Unlike monolith reactors with traversing channels, the triangular structure is made of radially translated layers of triangular channels which allows radial mixing and break-up of bubbles in between the layers. Up to 30–40% higher reaction rates in the whole range of the investigat-



Fig. 2. The ETH-designed semi-hydrogenation mini-plant installed in a DSM laboratory.

#### 3. Asymmetric Homogeneous Hydrogenation Reactions

The term vitamin E covers a group of compounds exhibiting similar biological activity to  $\alpha$ -tocopherol. They vary in the different degree of methylation on the aromatic ring and contain either a saturated or a threefold unsaturated aliphatic side chain. From an industrial point of view, the most relevant product of this class is (all-*rac*)- $\alpha$ -tocopherol, a lipid-soluble vitamin exerting an antioxidative effect that had a world-wide production volume of  $\geq$ 75,000 t in 2019.<sup>[12]</sup> (all-*rac*)- $\alpha$ -Tocopherol represents an equimolar mixture of all eight stereoisomers; however, the naturally occurring (R,R,R)-stereoisomer has the highest biological vitamin E activity. Therefore various investigations have been undertaken to achieve an industrially feasible synthesis of this compound. In particular, asymmetric hydrogenation was applied to introduce the stereogenic centres of the side chain by utilising the ruthenium-catalysed asymmetric hydrogenation of allylic alcohols.[13,14] For example geraniol and nerol can be hydrogenated at only the allylic position at up to S:C 50,000 to give citronellol containing up to 99% of the (3R) isomer.<sup>[15]</sup> Additionally, tetrahydrofarnesol **3** can be hydrogenated with S:C of up to 150,000 and selectivities of up to 98.6% at the newly-formed stereocentre of hexahydrofarnesol (R,R)-4.<sup>[16]</sup> The breakthrough development by Prof. A. Pfaltz of chiral iridium hydrogenation catalysts which do not require a neighbouring co-ordinating group for high selectivity<sup>[17]</sup> was the starting point for a long-standing cooperation in this area. In an earlier collaboration, such complexes were used in the hydrogenation of  $\gamma$ -tocotrienyl acetate 5, reducing three double bonds in one

step giving >98% of the desired stereoisomer (R,R,R)-6 (Scheme 3).<sup>[18]</sup> The same Ir-catalysts could also be successfully applied on farnesol and derivatives thereof.<sup>[19]</sup> These catalysts are unique as they allow the hydrogenation of purely alkyl-substituted and un-activated carbon–carbon double bounds in high selectivity.

Although excellent results were achieved with both approaches, none of them is industrially feasible since the synthesis of the substrates applied in the asymmetric hydrogenation can be laborious and is not cost competitive. A great step towards an industrially feasible synthesis of the (R, R, R)-isomer was achieved in a further cooperation with the research group of Prof. A. Pfaltz at the University of Basel aiming for an asymmetric hydrogenation of  $\gamma$ , $\delta$ -unsaturated ketones such as 7. These compounds can be easily obtained via industrialized approaches to the vitamin E side chain.<sup>[20]</sup> Since such substrates do not contain suitable coordination groups for Ru- or Rh-based catalysts, cationic iridium complexes (similar to those used for tocotrienol 5, Scheme 3) emerged as catalysts of choice. A screening of various catalysts revealed that the o-tolyl-derivatives delivered the highest selectivities in combination with a bulky substituent on the pyridine moiety. In particular, use of the anthracenyl substituted catalyst 9 resulted in 98.5% of the desired isomer of ketone 8 (Scheme 4).

Screening of various solvents revealed that an even higher selectivity can be reached; trifluoroethanol and catalyst **9** resulted in the formation of up to 99.1% of the desired stereoisomer, an *ee* >99% and a *dr* of 124:1. This methodology can be applied to different substrates obtained by minor variations in the process (Scheme 5). Besides (5*E*,9*E*)-farnesyl acetone **7**, different (*E*/*Z*)-

Scheme 3. Asymmetric hydrogenation approaches to the highly enantio-enriched tocopherol side chain.

Scheme 4. Hydrogenation of

was obtained for all entries.

(5*E*,9*E*)-farnesylacetone **7** with different bicyclic pyridine-based catalysts. Complete conversion



increasing selectivity

isomers,  $C_{13}$ -analogues and substrates containing only prochiral double bonds can be envisioned. Especially the last ones are of interest as a cheaper heterogeneous catalyst can be used to hydrogenate the non-prochiral double bond. The hydrogenation of these substrates resulted in similar selectivity compared to (5E,9E)-farnesyl acetone (7). If a double bond is present in (*Z*)- instead of the (*E*)-configuration, the stereogenic centre of opposite configuration is formed. Consequently, the saturated  $C_{18}$ -ketone **8** can be obtained not only in the desired (*R*,*R*)-form, but all four possible stereoisomers are accessible by the right choice of catalyst enantiomer and substrate.

The drawback of these catalysts is the requirement of the relatively high catalytic loading (minimum 0.1 mol%) for full conversion to the saturated ketones 8 and 10, meaning that such a process would not be commercially attractive. It was postulated that the ketone could be binding to the Ir-catalyst, leading to partial deactivation. Two ways were developed at DSM (a collaboration between the DSM sites in Switzerland and The Netherlands) to improve the turnover numbers of these hydrogenation reactions and therefore reduce the cost of the asymmetric hydrogenation. One was the use of a Lewis acid, such as an aluminium species.<sup>[21]</sup> Even more successful was the transformation of the ketone into a ketal which resulted in a significantly higher catalyst productivity, maintaining the high selectivity (Scheme 6). For (5E,9E)farnesylactone 7 only 27% of the fully saturated product 8 was obtained with a molar substrate to catalyst loading of 1,000 (the remainder was partially hydrogenated intermediates), whereas the corresponding ketal gave 98% of the fully hydrogenated compound with excellent (*R*,*R*) selectivity with half the amount of catalyst. Similar improvements in reactivity were obtained with the  $C_{13}$ -ketone **12**.<sup>[22]</sup> For reasons of speed, DSM decided to scaleup the unmodified hydrogenation of the unsaturated ketones in a stepwise manner, producing more than 5 kg of the  $C_{13}$ -ketone **10** and 1 kg of the  $C_{18}$ -ketone **8** using catalyst (*S*)-**11**, all in excellent yield and selectivity (Scheme 7).

#### 4. Acetophenone Synthesis by Solid-Acid Mediated Fries-Rearrangement

Hydroxyarylketones find widespread industrial applications, in particular *o*-hydroxyacetophenones **14** are interesting synthons in organic chemistry, and play an important role as intermediates in the pharmaceutical, fragrance and fine chemical industries. A general route to the 4-chromanone framework can be utilized to access intermediates for the synthesis of vitamin E.<sup>[23,24]</sup> One of the most common methods of synthesising *o*-hydroxyacetophenones is utilising the Fries rearrangement of phenyl acetates **13** (Scheme 8). This process is conventionally homogeneously catalysed by strong Lewis or Brønsted acids.<sup>[25]</sup>

Various heterogeneous catalysts have been evaluated in order to replace the often corrosive and toxic reagents, such as AlCl<sub>3</sub>, BF<sub>3</sub> or HF, and to avoid the formation of chemically reactive waste streams in stoichiometric amounts.<sup>[26]</sup> Limited information is, however, available on the substrate scope and, in particular, how different substitution patterns affect the yield and selectivity. We therefore started a systematic study on differently methyl-substituted phenyl acetates **13**,<sup>[27]</sup> with special emphasis on the use of heterogeneous catalysts.





In collaboration with Prof. J. Pérez-Ramírez at ETH Zurich, a broad range of materials was screened and the most promising results were obtained with zeolite catalysts, in particular those containing large-pore sizes such as beta zeolites. This indicated a structure-activity relationship enabling efficient conversion of certain dimethylphenyl acetates. The channel dimensions and the pore-size strongly influence the framework-dependent rearrangement vs. competitive ester cleavage pathway yielding the phenols 15 as by-products. For example, using a beta zeolite, 3,4-dimethylphenyl acetate 16 gave a 77:23 mixture of acetophenone:phenol, whereas 3,5-dimethylphenyl acetate 17 gave solely the corresponding phenol, with 15% by-products (Scheme 9).

Computational visualization at DSM of the molecular structures of both the reactants (phenyl acetates) and the surface of the catalysts indicated that the catalytic reaction may take place at the pore-mouth, taking into account steric factors. Reasonable conversions and selectivities for acetophenones were obtained with phenyl acetates of low steric bulkiness, whereas higher sub-



Scheme 9. Reaction of two differently substituted phenyl acetates catalysed by a beta zeolite.

#### 5. Selective Mono-Acetylation of a Vitamin A Intermediate

Vitamin A is important for the vision process, the immune system, and for healthy skin and is generally produced as the more stable acetate derivative. Several chemical routes to vitamin A acetate have been industrialized; in the DSM process, the intermediate diol (18) is acetylated on the primary alcohol to form 19, followed by elimination and isomerization to afford (all-*E*)-vitamin A acetate **21** (Scheme 10).<sup>[28]</sup> However, a significant amount of the diacetate 20 is also formed. Since higher yields can be obtained in the following steps if the pure mono-acetate is used, DSM was interested in exploring if a selective acetylation was possible using heterogeneous catalysts.[29]

The selective acylation was investigated in a research project with Prof. J. Pérez-Ramírez's group at ETH Zurich.<sup>[30]</sup> The homogeneous catalysed acetylation was first studied in more detail. When pyridine was applied as a basic catalyst, the mono-acetylated product (19) and the bis-acetylated product (20) formed in a ratio of about 3:1; the selectivity of acetylation could not be significantly influenced. The use of a heterogeneous catalyst could open new pathways that might achieve a higher mono-acetylation selectivity and it additionally would simplify the removal of the catalyst and its reuse. The use of hydrotalcites (layered double hydroxides) was chosen since it is possible to tune the catalyst by a number of variables in its synthesis. Medium and strong basic sites were varied by changing the Al-Mg ratio of the hydrotalcite; after preparation, the catalysts were thermally treated at temperatures ranging from 400 to 1,000 °C forming mixed metal oxides. The mesoporous structure of these compounds allows the bulky vitamin A intermediates to access the active sites of the catalyst. The catalysts were extensively characterized and activation at 700 °C resulted in maximum surface area of 161 m<sup>2</sup>/g. At higher temperatures the formation of spinel type structures was more favoured (with decreasing surface area).

The catalysts were applied in the acetylation of 18 under similar conditions as the pyridine catalysed acetylation. Non-thermally treated hydrotalcites showed a very high selectivity (nearly 100%) towards mono-acetylation under mild conditions, albeit with low conversions (<20%). The highest conversion (45%) was obtained with the hydrotalcite treated at 700 °C; the selectivity remained very high with only minor amounts of bis-acetylated product 20 being formed. The conversion could be improved by increasing the reaction temperature, with a small drop in selectivity. The var-



Scheme 10. Acetylation of an intermediate to vitamin A acetate.

iation of the Al-Mg ratio in the range from 1:1 to 4:1 also had an influence on both the activity and selectivity of the catalysts.

One advantage of using a heterogeneous catalyst is that it can be reused and this was studied in batch experiments. Over five runs, the yield of the mono-acetylated product **19** decreased slightly. XRD measurements showed that the structure of the mixed oxides changed slightly and organic deposits on the catalyst could be observed which were also a factor in the decreasing activity. However, the activity could be returned to almost the initial value by oxidative thermal treatment, removal of the organic deposits and restoring the initial mixed oxide structure. Overall it was demonstrated that a highly selective mono-acetylation could be achieved using heterogeneous catalysts derived from earth-abundant and non-toxic elements under mild reaction conditions.

#### 6. Oxidation Reactions

One key building block in the synthesis of vitamin E is 2,3,5-trimethylhydroquinone (TMHQ **25**). The compound is typically produced by oxidation of 2,3,6-trimethylphenol (2,3,6-TMP **22**) to 2,3,5-trimethylquinone (TMQ **24**), followed by hydrogenation to TMHQ **25** (Scheme 11).<sup>[12]</sup> However, most industrial processes currently require high loadings of environmentally problematic copper catalysts for the oxidation of phenols.<sup>[31,32]</sup>

DSM was interested in developing a safer, more environmentally friendly and cheaper process to TMQ **24**. One possibility would be the application of the catalytic photo-oxidation of phenols in benign solvents in continuous flow. As there was only limited experience of this technology in-house, we started a collaboration with the group of Prof. C. Sparr at the University of Basel. This is a good example of how DSM tackles such a problem in an early research phase.

DFT calculations were carried out at DSM to assess the reactivity of 2,3,5-TMP **23** and 2,3,6-TMP **22** towards singlet oxygen. The computed transition state energies indicated the kinetic feasibility of both reactions. The free energy barrier from 2,3,5-TMP compared to 2,3,6-TMP is about 2.0 kJmol<sup>-1</sup> lower, whereas the



Scheme 11. Synthesis of TMHQ **25** starting from 2,3,5-TMP **23** and 2,3,6-TMP **22**.

conformation of 2,3,6-TMP with the lowest energy possesses a slightly higher intrinsic free energy than 2,3,5-TMP in the ground state.

A photosensitizer screening was carried out at the University of Basel to confirm the DTF predictions and two starting phenol substrates were investigated. The most suitable photocatalyst for the oxidation of both substrates was methylene blue, producing good yields of 2,3,5-trimethylquinone **24** starting from both phenols.<sup>[33]</sup> This was a surprising and interesting result since in the copper-catalysed process, significantly lower yields are obtained using 2,3,5-TMP **23** compared to 2,3,6-TMP **22**.

The reaction conditions were further optimized and a photoreactor was designed and tested. The reactor consisted of 12 hyper red LEDs, an integrated CPU cooling system and the reaction mixture flowed through perfluoroalkoxy alkane (PFA) tubing wrapped around the light source (Fig. 3). 2,3,5-TMP was almost quantitatively converted in a 4:1 MeOH/H<sub>2</sub>O solvent mixture with 5 bar O<sub>2</sub> or 10 bar air and 0.9 mol% methylene blue to give a 96% yield of TMQ. A wide range of phenolic substrates could also be oxidized to their corresponding quinones, including 2-methylnaphthol to menadione **26** (vitamin K<sub>3</sub>), (Scheme 12). However, unsubstituted phenols and electron-deficient phenols remained unreacted.

Overall, a mild and sustainable synthesis of quinones and naphthoquinones was enabled by using a LED light source in a continuous-flow photoreactor using unproblematic solvents and short reaction times. Based on the successful results, the flow reactor developed in Basel has been installed in DSM's laboratories and further oxidation reactions are currently under investigation.



Scheme 12. Photochemical flow oxidation of phenols and naphthols to quinones and 1,4-naphthoquinones.



Fig. 3. Photoreactor designed and used for flow oxidation experiments. The light shielding aluminium foil is omitted for clarity. (Adapted from ref. [33], © 2021 Wiley-VCH GmbH)

## 7. (*R*)-Pantolactone (for Pantothenic Acid and Panthenol)

Pantothenic acid **28** (R = H), is also known as vitamin  $B_5$  and is important for the metabolism of carbohydrates, fats and proteins and also for the maintenance and repair of cells. It is predominately sold as its calcium salt for human and animal nutrition, and food and pharmaceutical use. The related D-panthenol **29** is used in pharmaceuticals, cosmetics and shampoos. The synthesis of both compounds use the same key intermediate, (*R*)-pantolactone (*R*)-**27** (Scheme 13). Currently all manufacturing routes start from the *rac*-pantolactone and perform a resolution.<sup>[34]</sup> We were interested in developing an improved and more sustainable asymmetric synthesis of (*R*)-pantolactone **27**. Different approaches were investigated at DSM, InnoSyn in the Netherlands and at the University of Basel.

An elegant route, using the existing *rac*-pantolactone (*rac*-27) would be a dynamic kinetic resolution, where the desired (*R*)-isomer would be acylated to produce (*R*)-30 and the undesired (*S*)-27 would be racemized *in situ* and then further converted to (*R*)-30. This has the potential for a '100% yield' process and uses a very cheap starting material (Scheme 14). A suitable racemization protocol was developed at DSM using the *Shvo*-catalyst<sup>[35]</sup> and a (*R*)-selective lipase was developed by InnoSyn and colleagues at DSM Delft (NL) by performing docking studies and site-selec-



Scheme 13. Preparation of calcium pantothenate and panthenol from (R)-pantolactone.

tive mutagenesis starting from the well-known *Candida antartica* lipase B (CalB) which showed low (R)-selectivity.<sup>[36]</sup> Although successful, the racemization required elevated temperatures and the lipase reaction was not selective enough, therefore this approach was put on hold.

An alternative concept is the reduction of ketopantolactone **31**. The asymmetric hydrogenation has been known for many years, based on work developed at Roche/DSM and elsewhere.[37] We investigated a number of modern asymmetric hydrogenation catalysts, but unfortunately could not find one with suitable reactivity and selectivity. Therefore we investigated the use of an enzymatic reduction, also in collaboration with InnoSyn (Scheme 15). One problem that was encountered was a significant, less selective, background reaction, resulting in lower ee's. Additionally, competing hydrolytic ring opening of the starting lactone 31 meant that the reduction could be occurring on the lactone, or the corresponding hydroxy acid, or both, potentially with different selectivities. A good protocol was developed with a keto-reductase at pH 5.5 resulting in ee's of >95%, but this required the use of the expensive NADPH as co-factor.<sup>[38]</sup> Slightly lower yields, but excellent selectivity were obtained with alternative enzymes.

Although successful, the synthesis of the starting ketopantolactone 31 could not be carried out in a cost-effective manner, so an alternative approach was investigated in a collaboration with the group of Prof. C. Sparr at the University of Basel. This involved an asymmetric organocatalysed condensation of isobutyraldehyde with a glyoxalate to give intermediate 32, which would then undergo aldehyde reduction and ring closure to give (R)pantolactone 27 (Scheme 16) in a sequential catalytic approach. Initial results showed that a hybrid (33) between D-proline and Noyori's TsDPEN ligand for catalytic transfer hydrogenation was successful for the aldol condensation and, after addition of [RuCl<sub>2</sub>(p-cymene)], and sodium formate, resulted in reduction and lactonization producing (R)-27 with 99% conversion and an er of 82:18.<sup>[39]</sup> The stereoselectivity was controlled by the chiral proline unit, since the corresponding ligand without the two phenyl groups (34) gave similar selectivity and even a proline-amino alcohol derived ligand 35 was the most selective. Performing the



Scheme 14. Dynamic kinetic resolution (DKR) approach to (*R*)-pantolactone acetate.



Scheme 15. Enzymatic reduction of ketopantolactone.



Scheme 16. Catalyst repurposing sequential catalysis approach to (R)-pantolactone.

transfer hydrogenation with  $[Ir(Cp^*)Cl_2]_2$  was even more successful resulting in an isolated yield of 84% with an *er* of 86:14 using just 0.1 mol% of the iridium complex.

Overall, the combination of in-house knowledge and investigations and collaborations with experts in particular fields, resulted in three new approaches to the important intermediate (R)pantolactone.

### 8. Vitamin E: From Bio-organic Chemistry to Catalytic Synthesis Methodology

The biocatalytic formation of (R,R,R)- $\alpha$ -tocopherol (RRR-37) was the starting point for a long-standing collaboration with the group of Prof. W.-D. Woggon at the University of Zurich and later at the University of Basel. The initial identification of the enzyme tocopherol cyclase was followed by studies of the reaction mechanism of the stereospecific chromanol ring formation and on substrate specificity,<sup>[40]</sup> as well as work on catalytic antibodies.<sup>[41]</sup> The biomimetic chromanol cyclization reaction of **36** (Scheme 17),<sup>[42]</sup> and of a structurally related substrate,<sup>[43]</sup> may be mentioned as a link between the biosynthesis and the organo/chemocatalytic synthesis of (R,R,R)-**37**. Several novel approaches for the highly stereoselective generation of the C(2) stereogenic centre were described<sup>[44]</sup> and comparatively reviewed.<sup>[45]</sup>

The methodology developed could also be used to gain additional knowledge about biologically interesting actions of vitamin E components and analogues. The asymmetric synthesis of nor- $\alpha$ tocopherol (in which the methyl group at position C2 is replaced by a hydrogen atom) enabled the discovery of biological activities beyond the established antioxidant properties.<sup>[46]</sup> The formation of high molecular weight oligomers of  $\alpha$ -tocopherol transfer protein was detected in a study led by the Stocker group at the University of Bern.<sup>[47]</sup> A study of the mobility of various vitamin E components in bio-membrane models by fluorescence quenching experiments was initiated by the Nau group at the University of Basel, and completed at the Jacobs University Bremen (Germany).<sup>[48]</sup>

In addition to collaborative projects with Swiss academic institutions, DSM has hosted a number of students from Switzerland and neighbouring countries to carry research projects as part of diploma, bachelor and master theses. In particular there are long-standing relationships with the Universities of Applied Sciences *e.g.*, the School of Life Sciences at Muttenz/ Basel and the Zurich University of Applied Sciences Winterthur,<sup>[49]</sup> mostly related to research in the area of vitamin E, and (+)-biotin.



Scheme 17. Biomimetic stereoselective chromanol ring formation.

In many of the examples mentioned above, some points of such collaborations should be mentioned going beyond the purely financial support of the industrial partner. For example, the supply of samples as starting material or as reference materials, which are not commercially available, *i.e.* stereoisomers, isotopically labelled compounds, or structurally related substances often not only help but even initiate certain aspects in an investigation. In addition, expert knowledge and advice on specific compound-classes has been provided that is not necessarily available in the open literature. Furthermore, support to academic partners can be performing specialized analytics and/or providing methods. Whilst there is no direct monetary value of this support, it may be invaluable for the success of a research project.

#### 9. Conclusions and Final Words

DSM has collaborated with a number of Swiss academics and institutions on a wide variety of topics. All the projects have been successful in one way or another; either by defining the scope and limitations of a particular transformation and/or catalyst, or developing new chemistry and synthetic routes to nutritional ingredients. We have seen examples above of new reactor concepts being developed and then brought in-house at DSM (e.g. continuous semi-hydrogenation and flow photochemistry), heterogeneous catalysts for selective reactions (acetylation and Fries rearrangement), new catalytic concepts (such as the catalyst repurposing sequential catalysis) and the development of processes to produce multi-kilograms of key intermediates (asymmetric hydrogenation). In addition to the valuable collaborations with Swiss academic institutions, DSM honoured to sponsor the Best Poster Presentation Awards at the SCS Fall Meeting providing to the students cash contributions, travel vouchers to attend international conferences, and invitations to present the research in an issue of Chimia. Overall, it has been an exceeding fruitful past decade and we look forward with great interest and expectation to the decades to come.

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